

### Pumping and Material Cost Analysis

The cost analysis was performed in order to find the best qualifying material; in this case a pumping cost analysis and a material cost analysis were performed. As shown in Table 14, the head loss was calculated for different material in order to find the pumping energy required for the specified flow demand. Table 15 shows the cost of energy of all materials in addition to the extra annual cost of each material compare to ductile iron pipe, and the present worth of those costs considering a fifty-year life expectancy.

Table 14 – Unit Head Loss Calculation for All Materials

Material	Q (GPM)	Diameter, (in)	Velocity, (ft/sec)	Roughness Coefficient, C	Unit Head Loss, (ft/kft)
DIP	5190.18	24.95	3.41	140	1.32
PVC	5190.18	22.76	4.09	150	1.82
PCCP	5190.18	24.00	3.68	140	1.59
HDPE	5190.18	20.83	4.89	155	2.63
STEEL	5190.18	24.00	3.68	140	1.59

Table 15 – Present Worth Calculation for Annual Cost

Material	Pumping Cost \$/yr/kft	Pumping Cost \$/yr/pipeline	Additional Cost \$	interest %	Present Worth \$
DIP	\$741.12	\$7,248.13	\$0.00	0.04	\$0.0
PVC	\$1,020.31	\$9,978.58	\$2,730.46	0.04	\$58,656.16
PCCP	\$895.38	\$8,756.76	\$1,508.63	0.04	\$32,408.76
HDPE	\$1,478.43	\$14,458.96	\$7,210.83	0.04	\$154,904.38
SP	\$895.38	\$8,756.76	\$1,508.63	0.04	\$32,408.72

As shown in Table 16, DIP has the most expensive unit cost. However, as mentioned previously in the report PVC and HDPE cannot be used because they do not meet requirements and specifications provided by EPWU. Moreover, PCCP and SP need

additional treatment for maintenance, corrosion control and cathodic protection, which will increase the total cost of the project. Therefore DIP is the best option.

Table 16 – Summary Table with Total Initial Cost

Material	Pipe Length, ft	Unit Cost, \$/lf	Total Material Installation Cost, \$	Present Worth, \$	Total Initial Cost, \$
DIP	9779.96	\$140.00	\$1,369,194.40	\$0.00	\$1,369,194.40
PVC	9779.96	\$99.00	\$968,216.04	\$58,656.16	\$1,026,872.20
PCCP	9779.96	\$110.00	\$1,075,795.60	\$32,408.76	\$1,108,204.36
HDPE	9779.96	\$110.00	\$1,075,795.60	\$154,904.38	\$1,230,699.98
STEEL	9779.96	\$120.00	\$1,173,595.20	\$32,408.72	\$1,206,003.92

### Conclusions

Based on this report analysis and after meeting all the objectives for the project, it was concluded that DIP was the most cost efficient and durable material. Not only does it meet all the requirements provided by EPWU and TCEQ, but also it is the material that requires the least amount of maintenance. Although the initial cost is not the most economical, ductile iron pipe has lower energy and pumping cost, which has proven to be the best option for the project.

References

- 290 citations for Emergency Preparedness Plans: 290 sub-chapter D. (n.d.). *TCEQ*. Retrieved November 19, 2011, from [www.tceq.texas.gov/assets/public/permitting/watersupply/pdw/290and291\\_citations\\_SB\\_361.pdf](http://www.tceq.texas.gov/assets/public/permitting/watersupply/pdw/290and291_citations_SB_361.pdf)
- Cement-Mortar Linings For Ductile Iron Pipe. (2006). DIPRA - Ductile Iron Pipe Research Association. Retrieved November 19, 2011, from <http://www.dipra.org/pdf/designOfDIP.pdf>
- Concrete Cylinder Pipe. (n.d.). *Hanson Pressure Pipe*. Retrieved November 19, 2011, from [www.hansonpressurepipe.com/index.php?option=com\\_content&view=article&id=](http://www.hansonpressurepipe.com/index.php?option=com_content&view=article&id=)
- Design of Ductile Iron Pipe. (2006). DIPRA - Ductile Iron Pipe Research Association. Retrieved November 19, 2011, from <http://www.dipra.org/pdf/designOfDIP.pdf>
- Ductile Iron Pipe Joints and Their Uses, (2006). *DIPRA - Ductile Iron Pipe Research Association*. Retrieved November 19, 2011, from <http://www.dipra.org/pdf/joints.pdf>
- Ductile Iron Pipe vs. HDPE Pipe . (2006). *DIPRA - Ductile Iron Pipe Research Association*. Retrieved November 19, 2011, from [www.dipra.org/pdf/DIPvsHDPE.pdf](http://www.dipra.org/pdf/DIPvsHDPE.pdf)
- Ductile Iron Pipe vs. PVC. (2006). *DIPRA - Ductile Iron Pipe Research Association*. Retrieved November 19, 2011, from [www.dipra.org/pdf/DIPvsPVC.pdf](http://www.dipra.org/pdf/DIPvsPVC.pdf)

Ductile Iron Pipe vs. Steel Pipe . (2006). *DIPRA - Ductile Iron Pipe Research Association*.

Retrieved November 19, 2011, from [www.dipra.org/pdf/DIPvsSteel.pdf](http://www.dipra.org/pdf/DIPvsSteel.pdf)

Hydraulic Analysis Of Ductile Iron Pipe. (2006). *DIPRA - Ductile Iron Pipe Research*

*Association*. Retrieved November 19, 2011, from

<http://www.dipra.org/pdf/hydraulicAnalysis.pdf>

Installation, Maintenance and Adjustment Instruction for Crosby® Series BP OMNI-

TRIM® Pressure Relief Valves. (n.d.). *Crosby Valve Inc.*. Retrieved November 19,

2011, from [www.hiter.com.br/arquivos\\_produtos/MIBPI.pdf](http://www.hiter.com.br/arquivos_produtos/MIBPI.pdf)

Means, R., Balboni, B., & Babbitt, C. (2011). *Heavy Construction Cost Data*. El Paso: R.S.

Means Company

MUTCD 2009 Edition, dated December 2009 (PDF) - FHWA MUTCD. (n.d.). *Manual on*

*Uniform Traffic Control Devices (MUTCD) - FHWA*. Retrieved November 19,

2011, from [http://mutcd.fhwa.dot.gov/pdfs/2009/pdf\\_index.htm](http://mutcd.fhwa.dot.gov/pdfs/2009/pdf_index.htm)

Seal, P., Insulator., Inc., & Houston. (n.d.). PSI Coated Metallic Casing Spacers provide

enhanced corrosion protection by way of a PVC Coating that is Fusion Bonded to

the surface of each casing spacer band. Coated Metallic Casing Spacer offer

runners with a low coefficient of friction to reduce the "push" or "pull" forces

required to insert large diameter (up to 120") heavy (ductile iron or cement coated

pipe) through casings. *PIPE AND PIPELINE PROTECTION BY USING*

*METALLIC AND NON-METALLIC CASING SPACERS AND ISOLATORS*.

Retrieved November 19, 2011, from [http://www.pipeline-seal.com/casing\\_isolato](http://www.pipeline-seal.com/casing_isolato)

SERIES 800 Butterfly Valves. (n.d.). GA Industries. Retrieved November 19, 2011, from [http://www.gaindustries.com/MProducts/Bulletins/ButterflyValves/50008\\_BFV800A.pdf](http://www.gaindustries.com/MProducts/Bulletins/ButterflyValves/50008_BFV800A.pdf)

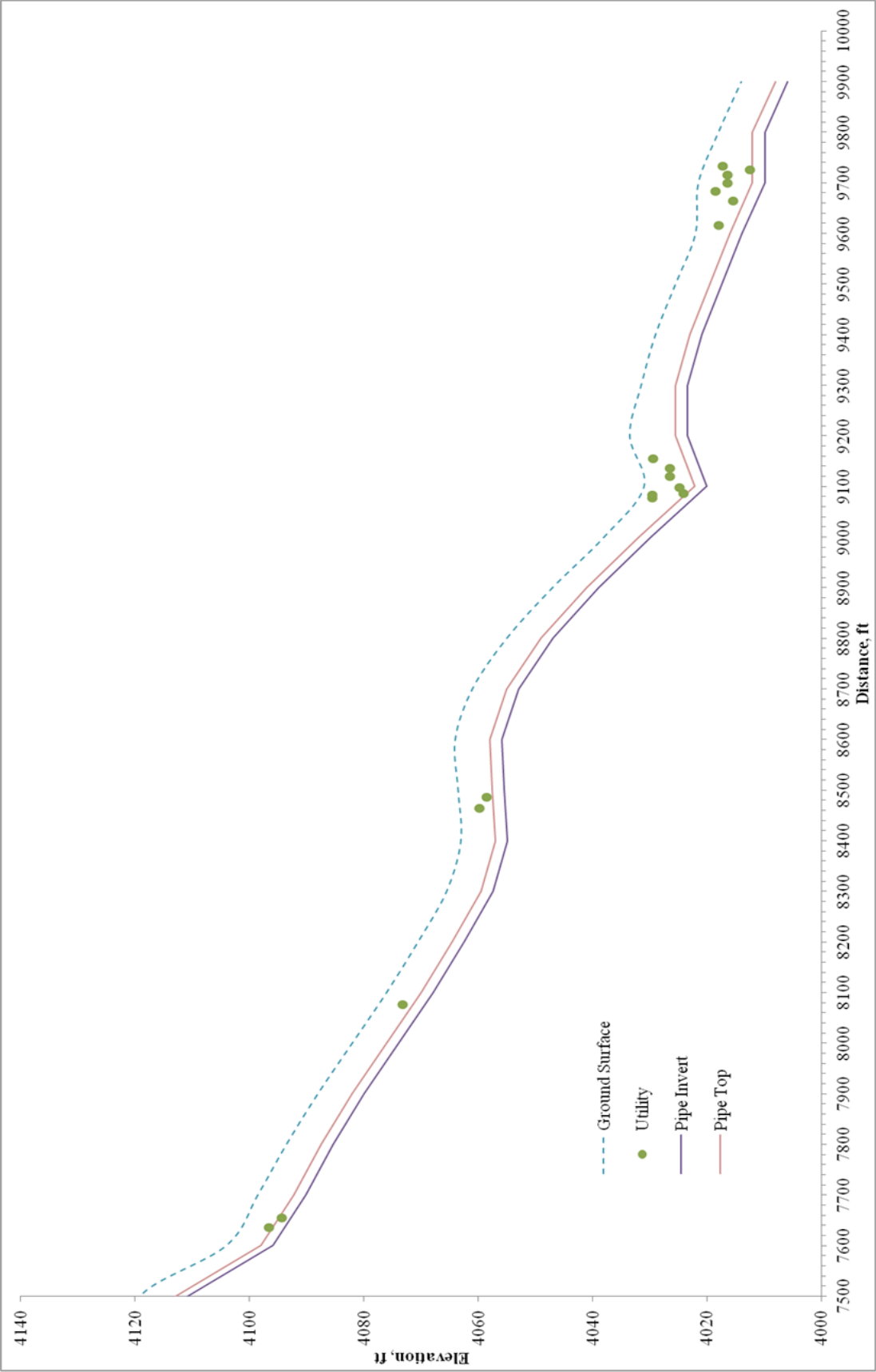
Swamee, P. K., & Sharma, A. K. (2008). *Design of water supply pipe networks*. Hoboken, N.J.: Wiley-Interscience.

Thrust Restraint Design for ductile iron pipe. (2006). DIPRA - Ductile Iron Pipe Research Association. Retrieved November 19, 2011, from <http://www.dipra.org/pdf/thrustrestraint.pdf>

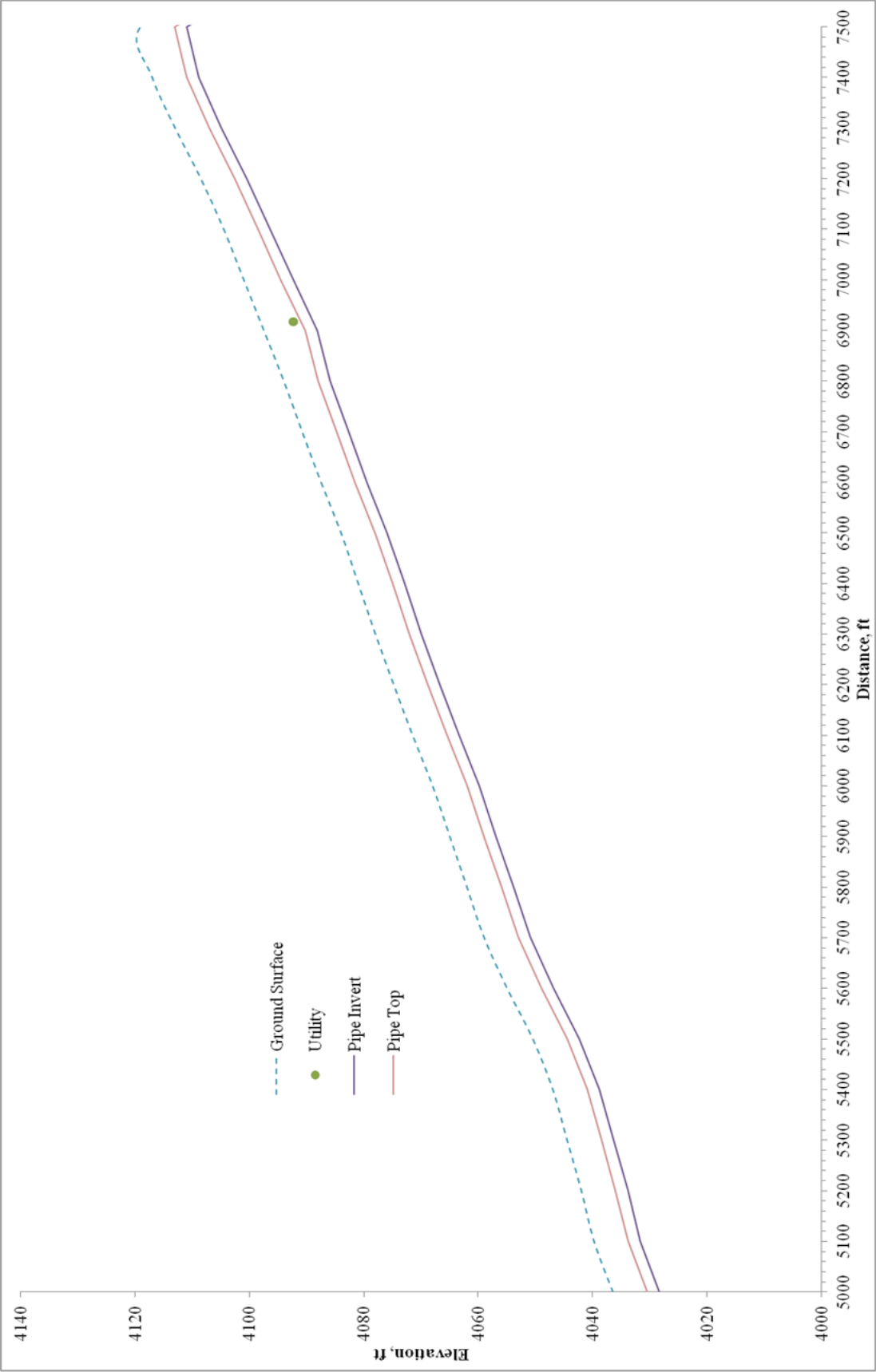
Vasquez, P.E., M. I. (2010). El Paso Water Utilities (EPWU) – Mesa Street 24” Water Line Replacement Project El Paso, El Paso County, Texas. *Geotechnical Soils Investigation Report, 1,7,8,9,10,11,18,30*.

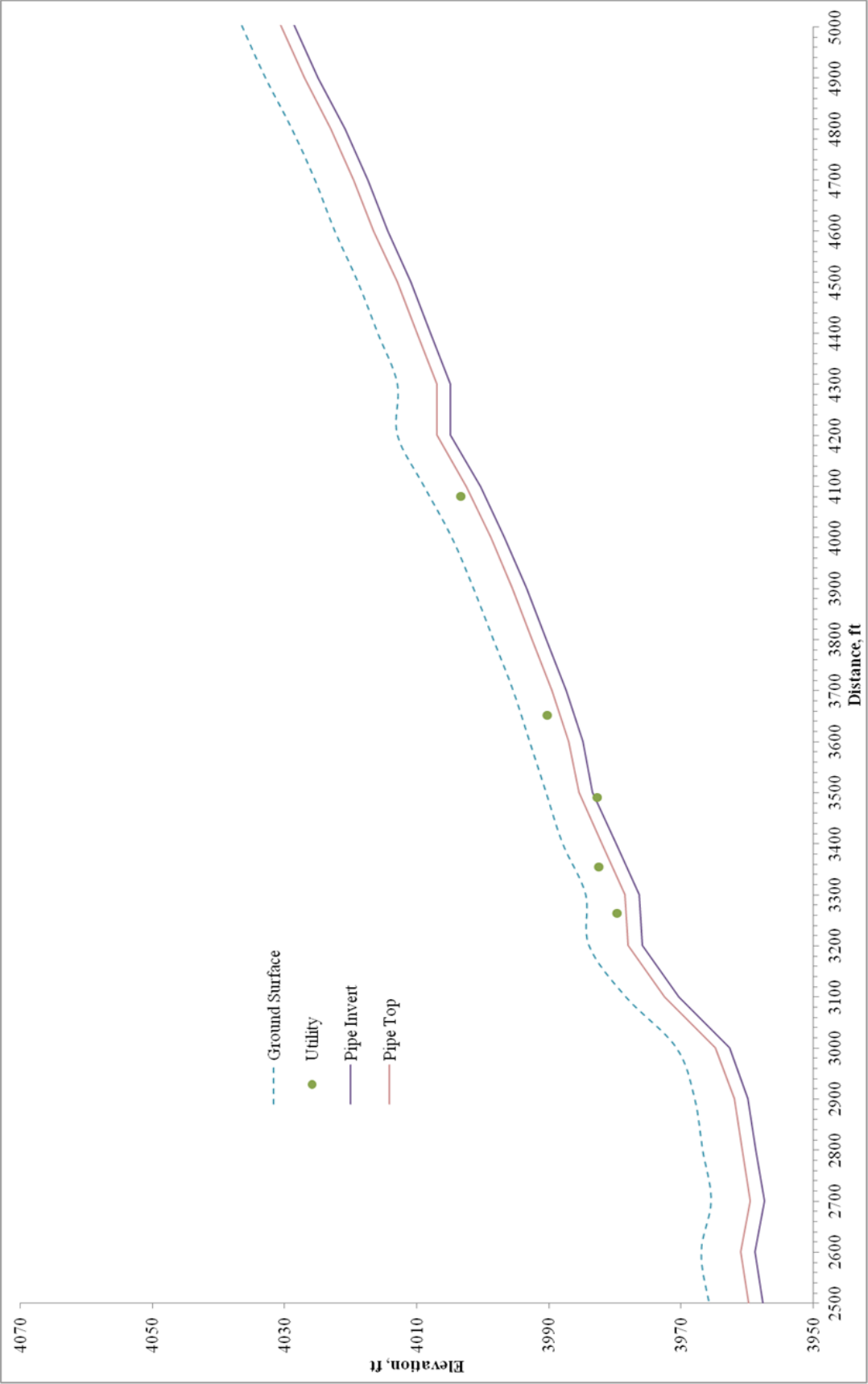
Vent-O-Mat. (2006, November). Air Release & Vacuum Break Valves. Series RBX Catalogue Index, 1, 2,3,4,5,11,12.

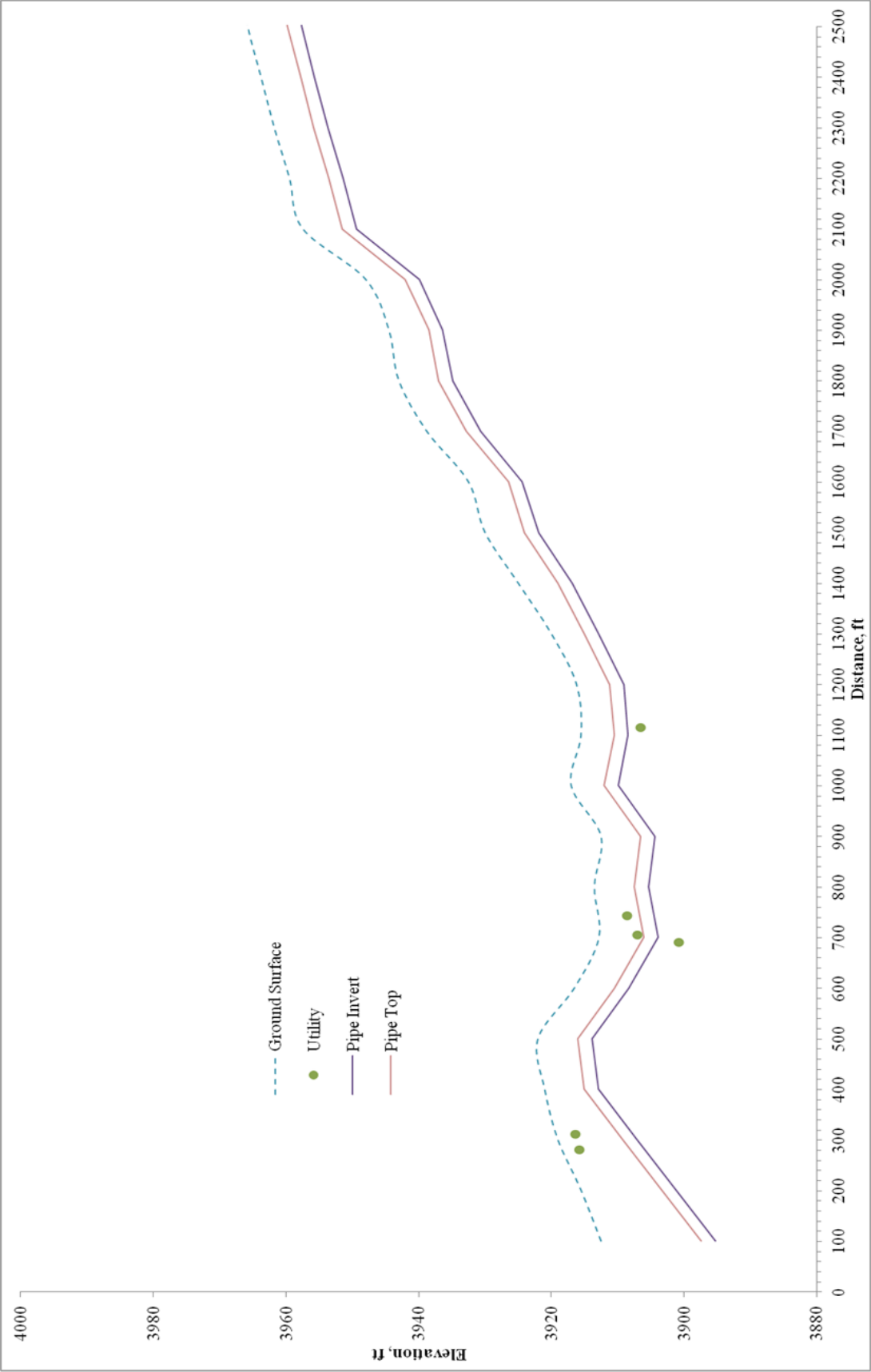
## Appendix



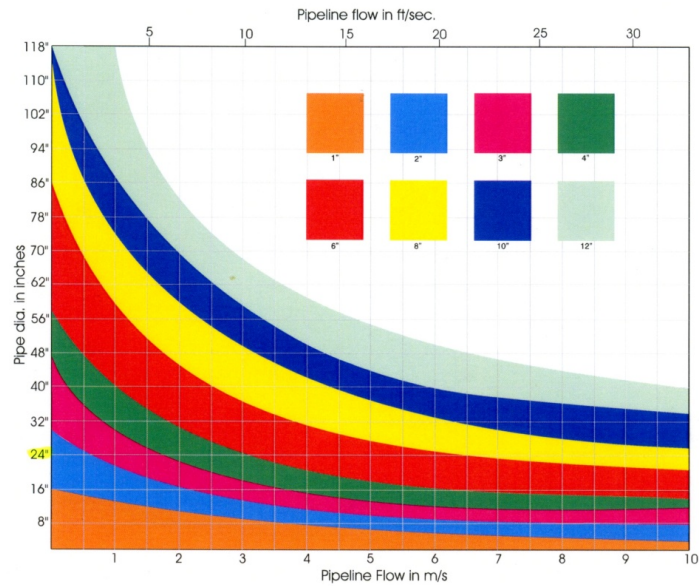








The selection for air release and vacuum relief valves was made in accordance to the graph below. This figure expresses the relationship between pipeline flow and pipe diameter yielding the required diameter for the valve.



Selection Graph for Diameter of Valves In Relationship with Pipeline Flow and Pipe Diameter

- Unit Bearing Resistance

$$R_s = D' * K_n * P_p$$

$P_p$  = Passive Soil Pressure

$D$  = Nominal Diameter

$K_n$  = Laying Condition

- Frictional Force

$$F_f = 0.7F_s \rightarrow \text{Polyethylene pipe}$$

$F_s$  = Unit Frictional Force

- Unit Frictional Force

$$F_s = A_p * C + W * \tan(\delta)$$

$A_p$  = Surface Area of Pipe Bearing on Soil

$C$  = Soil Cohesion

$W$  = Unit Nominal Force

- Surface Area of Pipe Bearing on Soil

$$A_p = \frac{D * \pi}{2} \quad (\text{For bends assumed half the pipe circumference bears against the soil})$$

$D$  = Diameter

- Soil Cohesion

$$C = F_c * F_s$$

$F_s$  = Unit Frictional Force

$F_c$  = Frictional Resistance Force

- Earth Load

$$W_e = \gamma_s(H + .11B_o) * B_o$$

$\gamma_s$  = Unit Weight of Soil

$H$  = Height

$B_o$  = Nominal Diameter